

Polymers for Temperature Independent Viscosity

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Abstract

Traditional oil-based drilling muds containing organoclay viscosifiers demonstrate a temperature dependent rheology. As the temperature of the mud decreases the viscosity goes up, and as the temperature of the mud increases, viscosity goes down. This phenomenon is particularly evident in offshore drilling where the fluid can experience temperatures of 40°F in the riser and temperatures of over 300°F at the bottom of the borehole. The dramatic differences in viscosity in the riser and near the bottom of the hole can lead to pressures exceeding the fracture gradient of the formation and other fluid management issues. A study was conducted to determine the effectiveness of two new flat rheology polymer chemistries at minimizing the rheological differences across a broad temperature range. The polymers were added to an organoclay containing mud and the before and after rheological properties were measured at 40, 100 and 150°F.

Rheological testing on the mud containing only organoclay showed a 65% decrease in YP and a 67% decrease in the 6 rpm reading from 40 to 150°F. The mud containing organoclay in addition to the flat rheology polymer showed only a 12% decrease in YP and no change in the 6 rpm reading from 40 to 150°F. PV was similar for both muds. The addition of the flat rheology polymer greatly eliminated the rheological change across the temperature range. This flatter rheology profile is ideal for offshore drilling.

Introduction

Drilling offshore presents challenges that are not encountered when drilling onshore. One of the biggest challenges is that the ocean temperature gradient and local geothermal gradient are both influential to the rheology of drilling fluids. As one goes deeper in the water column, temperatures decline. As one goes deeper in the ground, temperatures increase. Figure 1 illustrates this phenomenon. Conventional drilling fluids are temperature dependent, meaning that their rheology is influenced by the temperature experienced. The dramatic changes in temperature experienced when drilling offshore can cause controlling ECD and other fluid properties to become difficult or impossible. Drilling fluids which are temperature independent eliminate or drastically reduce fluid management issues.

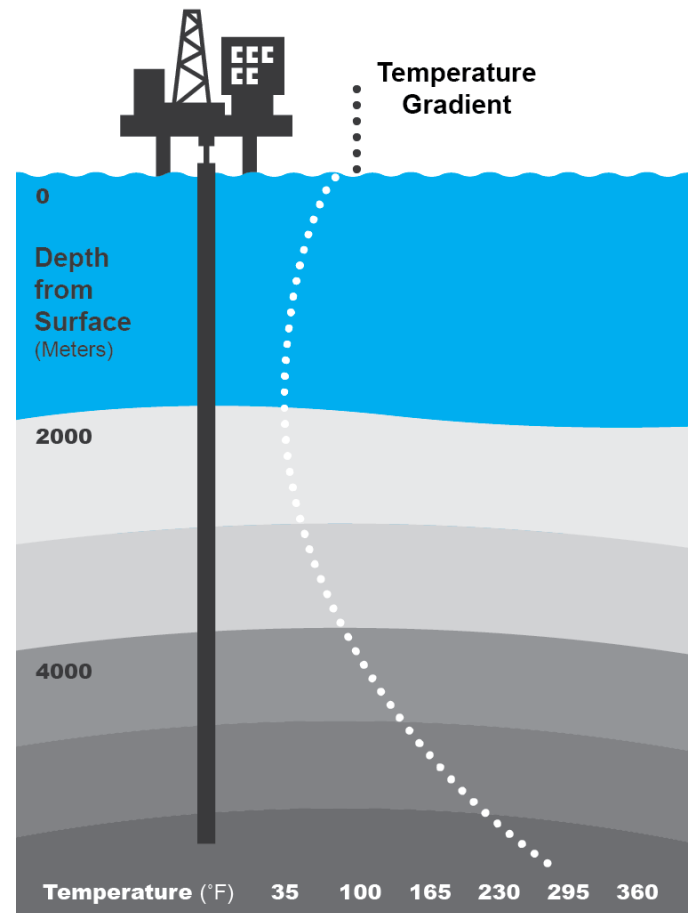


Figure 1. Typical offshore temperature gradient.

Conventional oil-based drilling muds containing organoclay viscosifiers demonstrate temperature dependent rheology. As the temperature of the mud decreases, the viscosity increases, and as the temperature of the mud increases, viscosity decreases. This phenomenon is particularly evident in offshore drilling, where the fluid can experience temperatures of 40°F in the riser and in excess of 300°F at the bottom of the hole. These differences in temperature cause differences in viscosity in conventional drilling fluids and can lead to exceeding the fracture gradient of the formation as well as other fluid management issues.

A study was conducted to determine the effectiveness of two new flat rheology polymer chemistries at minimizing the

rheological differences in oil-based drilling fluids across a broad temperature range. The polymers were added to organoclay containing mud. Rheology was measured at 150°F and then hot rolled at temperatures up to 250°F. Selecting the best flat rheology polymer chemistry for a drilling fluid depends on the amount of organoclay present in the fluid and the temperature that the fluid will experience at the bottom of the hole.

Polymer Chemistries

Two new polymer chemistries were developed to provide temperature independent rheology in OBM and were tested in the study.

The first polymer (Polymer 1) can be described as a solution of an alkyl-ammonium salt of a polycarboxylic acid. This chemistry was developed for drilling fluids which will not see BHT above 200°F and/or which have organoclay loadings below 2 lb/bbl.

The second polymer (Polymer 2) can be described as a solution of polyamine amides of unsaturated polycarboxylic acids. This chemistry was developed for drilling fluids which will see BHT above 200°F and/or which have higher loadings of organoclay.

Typical properties and solvent content of the two chemistries can be seen in Table 1.

Table 1. Properties of Polymer 1 and Polymer 2.

	Density at 68°F	Flash Point	Solvents
Polymer 1	0.97 g/ml	217.0°F	Propylene Glycol
Polymer 2	0.93 g/ml	109.4°F	C10-11 Isoparaffin and Butylglycol

Test Formulations and Experimental Methods

To study the effects of Polymer 1 and Polymer 2, two test fluid systems were prepared using commercially available materials. Both systems used the same synthetic base fluid, oil-to-water ratio, brine phase salinity, and surfactant package. The mud weights ranged from 12.0 to 13.0 ppg with oil to water ratios of 75/25. The internal phase was a 25% weight to volume calcium chloride brine. The brine was emulsified with a commercially available combination emulsifier/wetting agent package. The organoclay content ranged from 1-3 lb/bbl. API grade barite was used for the weighting agent as this would be worst case scenario in terms of sag. Lastly, 20 lb/bbl simulated drill solids were included in the system on the premise that they would be present in almost every case in the field: recycled mud or fresh drilling cuttings.

Each mud was evaluated for rheology and emulsion stability following API 13B-2 procedures for oil-based drilling fluids. Rheology and emulsion stability values were measured using an OFITE 900 viscometer and OFITE Emulsion Tester Model 131-50. Formulation 1 and Formulation 2 show the components and mixing order. After low shear mixing, the fluids were homogenized at 6,000 rpm until the fluid reached 150° F to ensure stability. The rheological properties were

measured at 150° F on a digital viscometer. The fluids were then transferred to heat aging cells, pressurized, and hot rolled overnight at 150 - 250° F depending on the test system.

Formulation 1. 13.0 ppg 75/25 Synthetic Based Mud

	lb/bbl	Mix Time (min)
C16-C18 Internal Olefin	148.6	
Organoclay	1	5
Lime	6	5
Emulsifier	15	5
25% CaCl ₂ Brine	83.7	10
API Barite 4.1	270	5
Simulated Drill Solids	20	5
Polymer 1	0 - 1.2	5
<i>High sheer on Silverson overhead mixer at 6,000 rpm until 150°F</i>		

After removing the cells from the roller oven, they were allowed to cool to ambient temperatures before venting and opening the cells. The cells were mixed and rheology was measured at several temperatures from 100 to 150° F. The mud contents were returned to the aging cell and re-mixed for five minutes. Finally, sufficient volume was poured into the chiller unit to obtain the 40° F rheology. The result summary of the testing on Formulation 1 can be seen in Table 1. Full testing results can be viewed in Appendix 1.

Table 1. Results for Formulation 1 After Hot Rolling for 16 Hours at 150°F.

Tests at 40°F	Organoclay Only	Organoclay and 1.2 lb/bbl Polymer 1
YP	29	16
6 rpm	14	11
10 min gel	14	17
Electrical Stability	N.M.	N.M.

Tests at 100°F	Organoclay Only	Organoclay and 1.2 lb/bbl Polymer 1
YP	14	14
6 rpm	8	11
10 min gel	8	15
Electrical Stability	N.M.	N.M.

Tests at 150°F	Organoclay Only	Organoclay and 1.2 lb/bbl Polymer 1
YP	12	15
6 rpm	5	11
10 min gel	5	18
Electrical Stability	412	864

Formulation 2 used a different flat rheology polymer that was designed to work with higher loadings of organophilic clays and at higher temperatures. In this round of testing, the amount of polymer was held constant at 0.6 lb/bbl while the organoclay content varied between 1 and 3 lb/bbl.

The muds were first hot-rolled overnight at 250° F. Then the mud were vertically static aged for 96 hours at 250° F. The muds were then re-homogenized for five minutes at 6,000 rpm on a Silverson mixer. The last step was to determine if the components degraded or the emulsion droplets increased in size during the static aging period. The result summary of the testing on Formulation 2 can be seen in Table 2. Full testing results can be viewed in Appendix 2.

Formulation 2. 12.0 ppg 75/25 Synthetic Based Mud

	lb/bbl	Mix Time (min)
C16-C18 Internal Olefin	148.6	
Organoclay	1-3	5
Lime	6	5
Emulsifier	15	5
25% CaCl ₂ Brine	83.7	10
API Barite 4.1	190	5
Simulated Drill Solids	20	5
Polymer 2	0.6	5
<i>High sheer on Silverson overhead mixer at 6,000 rpm until 150°F</i>		

Table 2. Results for Formulation 2 after Static Aging for 4 Days at 250°F.

Tests at 40°F	1 lb/bbl Organoclay and 0.6 lb/bbl of Polymer 2	2 lb/bbl Organoclay and 0.6 lb/bbl of Polymer 2	3 lb/bbl Organoclay and 0.6 lb/bbl of Polymer 2
YP	9	11	17
6 rpm	4.9	6.0	9.1
10 min gel	5	7	11
Electrical Stability	N.M.	N.M.	N.M.

Tests at 120°F	1 lb/bbl Organoclay and 0.6 lb/bbl of Polymer 2	2 lb/bbl Organoclay and 0.6 lb/bbl of Polymer 2	3 lb/bbl Organoclay and 0.6 lb/bbl of Polymer 2
YP	5	8	13
6 rpm	3.2	5.4	9.1
10 min gel	5	6	10
Electrical Stability	175	279	407

Conclusions

Offshore drilling conditions create difficulties in managing drilling fluid properties, especially with respect to rheology. Combinations of temperature independent polymers and organoclays can be used to create viscosity profiles which vary little across the expected operating temperature range. The choice of polymer depends on the amount of organoclay required in the system as well as the maximum expected exposure temperature of the drilling fluid. Polymer 1 works very well in systems where less than 2.0 lb/bbl of organoclay is used and where maximum temperatures will not exceed 200°F. Polymer 2 showed better performance in fluids that contained higher levels of organoclay necessary for reducing barite sag and in fluids that will experience temperatures greater than 200°F.

Both of these flat rheology polymers include an oil wetting component which often generates higher ES values. Moreover, as flat rheology systems tend to employ high loading levels of emulsifiers, it is worth comparing the aged systems before and after re-shearing. As seen in this study, the components are still functional.

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Nomenclature

Organoclay	=quaternary ammonium compound treated clay
°F	=Degrees Fahrenheit
YP	=Yield Point
PV	=Plastic Viscosity
ppg	=pounds per gallon
lb/bbl	=pounds per barrel
75/25	=volume ratio of 75% base fluid and 25% brine
N.M.	=Not Measured
OBM	=Oil-base Mud

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Appendix 2. Full Test Results for Formulation 2.

Organoclay	1 lb/bbl		2 lb/bbl		3 lb/bbl	
Polymer 2	0.6 lb/bbl		0.6 lb/bbl		0.6 lb/bbl	
Test Temp. (°F)	40°	120°	40°	120°	40°	120°
Before Hot Rolling						
600 rpm	132	66	144	73	167	82
300 rpm	74	41	82	47	96	54
200 rpm	55	33	61	38	71	44
100 rpm	34	23	39	27	46	32
6 rpm	9.0	10.1	11.2	12.4	13.7	16.5
3 rpm	8	9	9	11	12	15
PV	57	24	62	26	71	28
YP	17	17	21	21	25	26
10 sec gel	8	9	9	11	12	15
10 min gel	9	9	12	13	15	17
ES	–	519	–	616	–	756
Muds static aged at 250°F for 4 days						
600 rpm	122	48	142	56	158	65
300 rpm	66	27	77	32	88	39
200 rpm	47	20	54	25	63	30
100 rpm	27	13	31	16	38	21
6 rpm	4.9	3.2	6.0	5.4	9.1	9.1
3 rpm	4	3	5	5	8	9
PV	56	22	65	24	71	26
YP	9	5	11	8	17	13
10 sec gel	4	3	5	5	8	7
10 min gel	5	5	7	6	11	10
ES	–	175	–	279	–	407
Silversoned at 6,000 rpm for 5 minutes						
600 rpm	124	56	137	63	151	70
300 rpm	72	36	79	40	88	45
200 rpm	53	28	60	32	67	36
100 rpm	34	20	39	23	43	27
6 rpm	9.6	8.1	12.6	10.1	15	12.3
3 rpm	8	8	11	9	14	12
PV	52	21	58	23	63	25
YP	20	15	22	18	25	20
10 sec gel	9	8	12	9	14	12
10 min gel	12	9	15	11	18	14
ES	–	471	–	558	–	667

Appendix 1. Full Test Results for Formulation 1.

	Base Mud			1.2 lb/bbl Polymer 1		
Test Temp. (°F)	40°	100°	150°	40°	100°	150°
Before Hot Rolling						
600 rpm	200	83	55	179	91	65
300 rpm	120	49	34	102	58	44
200 rpm	91	38	26	76	46	36
100 rpm	60	27	18	49	33	27
6 rpm	18	10	6	15	16	15
3 rpm	15	8	5	13	15	14
PV	80	34	21	77	33	21
YP	39	15	14	25	24	22
10 sec gel	15	8	5	14	10	14
10 min gel	16	9	5	19	16	18
ES	–	–	572	–	–	742
After Hot Rolling 150° F						
600 rpm	185	89	53	195	89	63
300 rpm	107	51	32	106	52	39
200 rpm	80	39	24	75	40	31
100 rpm	51	26	16	45	27	22
6 rpm	14	8	5	11	11	11
3 rpm	11	7	4	10	10	10
PV	78	38	21	90	38	24
YP	29	14	12	16	14	15
10 sec gel	11	7	4	11	9	11
10 min gel	14	8	5	17	15	18
ES	–	–	412	–	779	864
After Hot Rolling 250° F						
600 rpm	168	75	50	176	81	56
300 rpm	92	42	29	95	46	33
200 rpm	66	31	21	68	35	25
100 rpm	40	20	14	40	23	17
6 rpm	9	6	4	10	8	7
3 rpm	7	5	3	8	7	6
PV	76	33	21	81	35	23
YP	17	8	9	15	12	10
10 sec gel	7	5	3	9	7	6
10 min gel	7	5	3	11	10	9
ES	–	385	219	–	530	595