

Corrosion Resistant Alloys in CO₂ Injection Wells for CCS and CCUS Projects

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Presenter: Adam C. Rowe, PE
Principal
Metallurgical Engineer
Stress Engineering Services, Inc.

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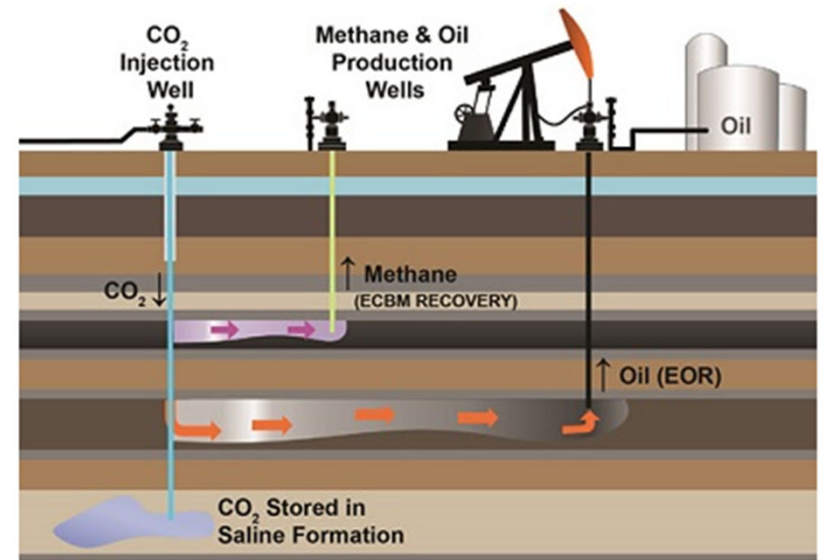
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To request any information contained in this presentation, please contact: Adam Rowe at adam.rowe@stress.com.



What is CCS and CCUS?

- Carbon capture and sequestration (CCS)
- Carbon capture utilization and storage (CCUS)
- This presentation will focus on CO₂ injection well metallurgy for storage wells



Source: <https://netl.doe.gov/carbon-management/carbon-storage/faqs/carbon-storage-faqs>

So What's the Problem?

- CO₂ pipelines have been successfully developed for many years without corrosion
- Pipelines are typically carbon steel
- No water → No corrosion
 - Carbon and low alloy steel okay
- Free water → Severe corrosion
 - CRAs needed
- Possible sources of water
 - Condensation
 - Formation water
 - Flowback



Corrosion Assessment

- Major challenge → Limited data for many CRAs in SC-CO₂
- Can lean on related experience for guidance with significant limitations
 - Oil and gas production – No oxygen
 - Acid gas injection – Lower temperature, No oxygen
 - Seawater injection – Near neutral pH
 - CO₂ EOR
 - CCS wells are often deeper and hotter
 - CCS utilizes continuous injection, no WAG
 - CCS wells typically have longer design lives
 - CCS injectate may have additional contaminants



Factors that Impact Corrosion in SC-CO₂

- Injectate composition and impurities in the SC-CO₂ stream
 - H₂S, O₂, SO_x, NO_x, H₂
- Water / water chemistry
 - No water → No corrosion
 - Fresh condensate → No buffering, no chlorides
 - Formation water → Buffering, chlorides
- Temperature
 - Important, but impact substantially dependent on other factors
 - Generally, higher temperature → higher corrosion rates to CRAs
- pH
 - Directly related to CO₂ pressure / fugacity
 - Generally, lower pH → higher corrosion rates

SC-CO₂ Stream Impurities

- Impurity contents vary substantially by source
- H₂S, O₂, SO_x, NO_x of utmost interest for material selection
- Examples shown below, but many other sources and compositions exist
- These ranges are too broad for material selection criteria
 - Actual project stream specification needs to be considered

Data Source	Industries	Typical Impurities
IPCC Special Report	Power Generation – Coal Fired Plants	0-0.5% SO ₂ , 0-0.01% NO, 0-0.6% H ₂ S, 0.01-3.7% N ₂ /Ar/O ₂
IPCC Special Report	Power Generation – Gas Fired Plants	< 0.01% SO ₂ , < 0.01% NO, < 0.01% H ₂ S, 0.01-4.1% N ₂ /Ar/O ₂
Industry Experience	Natural Gas Processing	< 1% H ₂ S, < 10 ppm O ₂
Industry Experience	Ethanol plants	< 10 ppm H ₂ S, < 2% O ₂



Effect of SC-CO₂ Stream Impurities

- SO_x and NO_x
 - Sulfuric acid and/or nitric acid formation in water phase
 - pH reduction
 - When present together, NO₂ catalyzes oxidation of SO₂
- H₂S
 - Can promote cracking susceptibility
 - Has not been rigorously studied in SC-CO₂
 - ISO 15156 best available guideline
 - Based on experience in oxygen-free oilfield environments
- O₂
 - Dissolved oxygen in the water phase promotes susceptibility to pitting and crevice corrosion
 - Perhaps most significant difference between CCS and oil and gas production environments
 - PREN helpful tool for ranking stainless steels
 - $PREN = \%Cr + 3.3 \times (\%Mo + 0.5\%W) + 16 \times \%N$
 - Relationship has not been established between PREN and corrosion resistance in SC-CO₂ environments
- Nitrogen (N₂) and Hydrocarbons not expected to influence material selection
 - Possible effects of Hydrogen (H₂) in CCS streams has not been explored and may warrant review

Mixtures of H₂S and O₂ can also form elemental sulfur!

Alloy	PREN (Typical)
13Cr	13
304 SS	18
316 SS	23
22Cr DSS	36
25Cr SDSS	42



Formation Water

- For CRA selection, chloride is the critical constituent
- Chloride can vary substantially from formation to formation
 - Also sample to sample and test to test
- Ideally, material selection based on water analyses from several samples
- Sometimes preliminary recommendations are needed based only on estimated TDS
 - Conservative assumption is that TDS is entirely NaCl
- Formation water pH shown is BEFORE injection

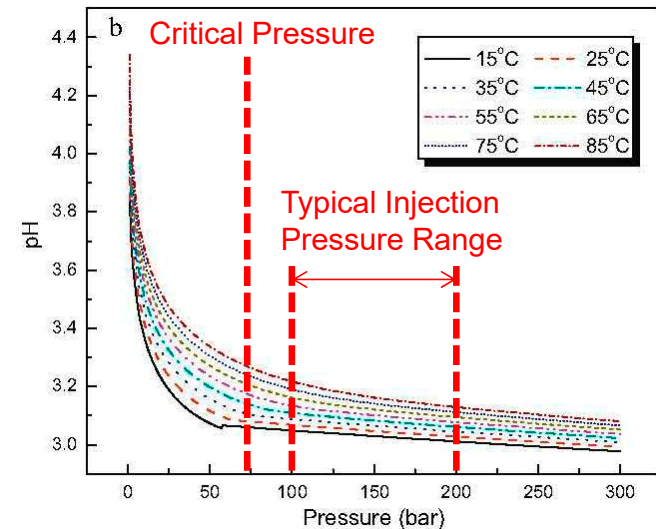
Species	Compiled by Zerai [CWRU, 2006]				For Reference*
	Rose Run	Clinton	Mt. Simon	Grand Rapids	Typical Seawater
	mg/kg	mg/kg	mg/kg	mg/kg	mg/kg
Na ⁺	60,122	67,000	32,000	26,539	10,561
K ⁺	3,354	850	1,060	636	380
Ca ²⁺	37,600	23,200	12,400	2,737	400
Mg ²⁺	5,881	1,840	2,190	533	1,272
HCO ₃ ⁻	122	200	71	182	142
Cl ⁻	191,203	160,400	78,700	47,549	18,980
SO ₄ ²⁻	326	523	1,180	337	2,649
Sr ²⁺	456	753	236	-	13
pH	6.4	6.5	6.7	7.2	8.2
TDS	277,571	250,000	150,000	90,000	~34,000

*Source: NACE Corrosion Engineer's Reference Book



pH Considerations

- As CO₂ pressure increases, the pH of present freshwater approaches 3
 - Can be demonstrated by modeling
- Adding as little as 100 ppm SO₂ can drop pH to 2.5
 - Recall that streams from coal-fired plants may have up to 5000 ppm SO₂
- These pH values are lower than most available corrosion data from oil and gas wells



Source: <http://www.icmt.ohio.edu/documents/publications/8253.pdf>

pH Considerations (cont.)

- Injection plume models have predicted that the pH near the wellbore will remain low even after many years
- pH increases with distance from the wellbore due to dilution and buffering
- Monitoring wells may therefore see higher pH, and different metallurgy may be suitable



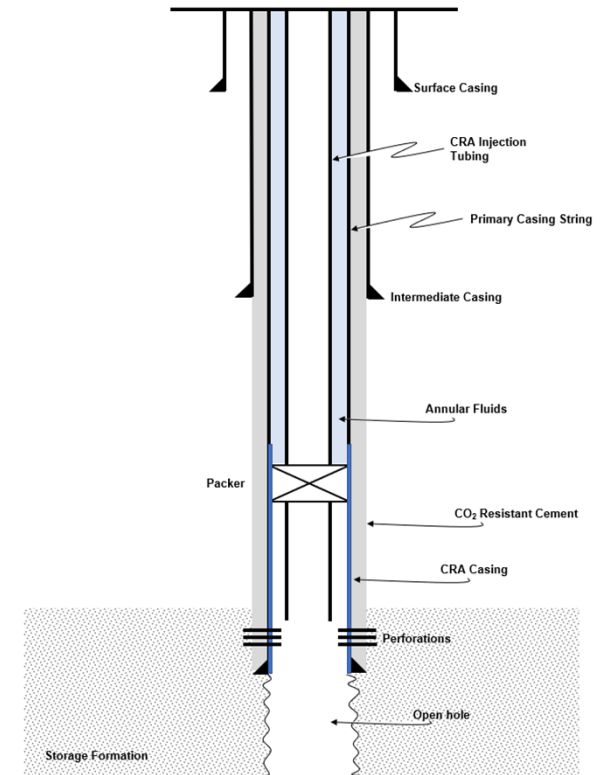
Candidate Alloys – Many Options Available

- Casing and Tubing
 - Carbon and Low-alloy Steel
 - 13Cr/S13Cr
 - 15Cr/17Cr
 - 22Cr
 - 25Cr
 - Higher Cr options
 - Nickel-base (G3/2550/C22)
 - Titanium
- Packers and Tubing Hangers
 - Carbon and Low-alloy Steel
 - 22Cr and 25Cr – limited strength
 - PH Ni-base alloys
 - Titanium
- Wellheads/Trees
 - Low alloy steel – No water drop out
 - Class CC – Limited acceptable options
 - Class HH



How to Select? Material Selection Philosophy

- Can exposure to water be reliably avoided over the life of the well?
 - If so, then carbon steel may be acceptable
 - Applies to non-wetted portions of the tree/wellhead and properly cemented casing above the packer
- Intermittent water warrants a risk assessment
 - Very corrosive when present
 - Balance equipment integrity against workover schedule
- Frequent or continuous water exposure requires CRA
 - Which CRA to choose?
 - Water from condensation or formation?
 - Cost typically increases substantially with corrosion resistance
 - Consultation with a Subject Matter Expert (SME) is needed



Martensitic Stainless Steels

- 13Cr, S13Cr, 15Cr, 17Cr
 - Strengthened by heat treatment, quenched and tempered
- 13Cr is commonly used in oil and gas production
 - AISI 420, L80 Type 13Cr
 - Available test data suggests that it is questionable for SC-CO₂, even without the presence of oxygen
- S13Cr
 - Alloyed with Mo for improved corrosion and cracking resistance
 - Better pitting resistance than 13Cr, but still limited in CCS environments
- 15Cr and 17Cr
 - No publicly available data in SC-CO₂
 - May be suitable in low O₂ – testing recommended
- Cracking resistance of these alloys has not been established at low pH expected in CCS when H₂S is present
- Possible application in monitoring wells, but Subject Matter Expert review is recommended



Duplex Stainless Steels

- 22Cr (e.g. SAF 2205, SM22CR, VM 22)
 - Good experience in oil and gas
 - Limited in H₂S and O₂ bearing streams
- 25Cr (e.g. SAF 2507, SM25CR/CRW, VM 25S)
 - Exhibits some pitting resistance in dissolved oxygen
 - Demonstrated by good industry experience in offshore equipment and seawater injection
 - Critical pitting and crevice corrosion temperatures well established in saturated seawater and acidified ferric chloride
 - CCS limits not established
- Very limited CCS data available for 22Cr and 25Cr
- No public data for higher Cr DSS such as 3207
- Strengthened by cold-work, so may not be suitable for high strength hangers and packers with thick sections

CPT and CCT for Select CRAs in Seawater

Alloy	CPT, °C	CCT, °C
304 SS	2	-15
316 SS	10	-10
22Cr DSS	40	20
25Cr SDSS	80	70



Nickel Alloys

- Solid solution and cold-worked alloys for tubing and casing
 - Alloys 2535, G3, 2550, C276, C22
 - Tubulars may be offered in grades up to 125 ksi SMYS
- Precipitation-hardened (PH) alloys
 - Alloys 925, 718, 725, 625 Plus
 - Strengthened by heat treatment
 - PH nickel alloys may be needed for higher strength packers and hangers
- Almost no publicly available CCS data
 - Some CCS combinations of low pH, high T, and high O₂ may still be pitting risk



Common Questions

- Will galvanic corrosion be a concern?
- Will this new alloy that my supplier is suggesting work for my well?
- What thread should we use for our downhole connections?
- What material requirements should we specify to the mill?
- Classic metallurgist response: “*It Depends!*” ㄟ_(_ツ)_/
- These are all good questions that need to be carefully considered on a project-by-project basis with the input from subject matter experts from several disciplines

Other Considerations

- Injection rates
 - Consideration of critical erosional velocities
- Threaded connections
 - Gas-tight premium connections
 - Risk of low temperature event?
- Annular fluids
 - Typically halide brines with additive package including oxygen scavengers
 - Need to be compatible with CRA
 - Can become aggressive if comingled with CO₂ stream
- Acid jobs
 - Possible damage to equipment if not quickly circulated out
- Elastomers
 - Sealing elements used for production equipment may not be compatible in SC-CO₂
- Cements
 - Portland cement is not compatible with CO₂
 - Need CO₂-resistant cement for exposed portions of well



Final Thoughts on CO₂ Injection Well Metallurgy

- The information presented here is intended to bring attention to the parameters that need to be considered in material selection
- It is always recommended that material selection and procurement specifications be reviewed by a Subject Matter Expert prior to ordering equipment
- Free water is the most critical factor in a corrosion assessment, and standard steel construction is suitable so long as the water stays completely soluble in the supercritical CO₂ for the life of the well
- When free water is determined to be present, material selection should be reviewed by a Subject Matter Expert and should carefully consider the following:
 - The composition of the injectate and maximum allowable impurities in the stream
 - The composition of water in the injection zone, such as a saline formation
 - Maximum injection pressures and bottomhole temperatures



Industry Needs as CCS Continues to Grow

- More corrosion data in SC-CO₂ environments
 - 2023 is expected to yield a large volume of new tests data
 - Temperature and impurity limits will need to be established for many CRAs
- Material selection guidelines
 - Currently, only a couple papers have been published touching on material selection guidelines for CCS injection wells
 - The PCOR Partnership and Stress Engineering have recently developed more comprehensive guidelines for CCS injections wells
 - Publication is in progress
- More field experience and case studies



Thank You!

